## Principles and Practice of Cleaning in Place

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- Principles of CIP
- CIP Detergents
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- Monitoring/Control



# CIP / SIP - Definition

#### • CIP = Cleaning in Place

To clean the product contact surfaces of vessels, equipment and pipework in place.
 i.e. without dismantling.

- SIP = Sterilise in Place
  - To ensure product contact surfaces are sufficiently sterile to minimise product infection.



# How CIP Works

Mechanical

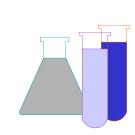
– Removes 'loose' soil by Impact / Turbulence

- Chemical
  - Breaks up and removes remaining soil by Chemical action
- Sterilant/Sanitiser
  - 'Kills' remaining micro-organisms (to an acceptable level)



### Factors affecting CIP

- Mechanical
- Chemical



- Temperature
- Time







# **CIP** Operation

- PRE-RINSE
  - Mechanical Removal of Soil
- DETERGENT
  - Cleaning of Remaining Soil
  - Caustic, Acid or Both
- FINAL RINSE
  - Wash Residual Detergent/Soil
- STERILANT/SANITISER
  - Cold or Hot



# **Typical CIP Times**

	Vessel CIP	Mains CIP
Pre-Rinse	10 to 20 mins	5 to 10 mins
Caustic Detergent	30 to 45 mins	20 to 30 mins
Rinse	10 to 15 mins	5 to 10 mins
Acid Detergent	20 to 30 mins	15 to 20 mins
Rinse	15 to 20 mins	10 to 15 mins
Sterilant	10 to 15 mins	5 to 10 mins



# **Typical CIP Temperature**

- Brewhouse Vessels
- Brewhouse Mains
- Process Vessels
- Process Mains
- Yeast Vessels
- Yeast Mains

Hot 85°C Hot 85°C  $Cold < 40^{\circ}C$ Hot 75°C Hot 75°C Hot 75°C



# CIP Detergent -Requirements

- Effective on target soil
- Non foaming or include anti-foam
- Free rinsing / Non tainting
- Non corrosive Vessels/pipes, joints
- Controllable Conductivity
- Environmental



## **Caustic Detergents**

- Advantages
  - Excellent detergency properties when "formulated"
  - Disinfection properties, especially when used hot.
  - Effective at removal of protein soil.
  - Auto strength control by conductivity meter
  - More effective than acid in high soil environment
  - Cost effective

- Disadvantages
  - Degraded by CO<sub>2</sub> forming carbonate.
  - Ineffective at removing inorganic scale.
  - Poor rinsability.
  - Not compatible with Aluminium
  - Activity affected by water hardness.



#### Acid Detergents

- Advantages
  - Effective at removal of inorganic scale
  - Not degraded by CO2
  - Not affected by water hardness
  - Lends itself to automatic control by conductivity meter.
  - Effective in low soil environment
  - Readily rinsed

- Disadvantages
  - Less effective at removing organic soil.
     New formulations more effective.
  - Limited biocidal properties -New products being formulated which do have biocidal activity
  - Limited effectiveness in high soil environments
  - High corrosion risk Nitric Acid
  - Environment –
     Phosphate/Nitrate discharge

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### **Detergent Additives**

- Sequestrants (Chelating Agents)
  - Materials which can complex metal ions in solution, preventing precipitation of the insoluble salts of the metal ions (e.g. scale).
  - e.g. EDTA, NTA, Gluconates and Phosphonates.
- Surfactants (Wetting Agents)
  - Reduce surface tension allowing detergent to reach metal surface.



# Sterilant / Sanitiser Requirements

- Effective against target organisms
- Fast Acting
- Low Hazard
- Low Corrosion
- Non Tainting
- No Effect On Head Retention
- Acceptable Foam Characteristics



## Sterilants / Sanitisers

- Chlorine Dioxide
- Hypochlorite
- Iodophor
- Acid Anionic
- Quaternary Ammonium
- Hydrogen Peroxide
- PAA (Peroxyacetic Acid) 200-300 ppm

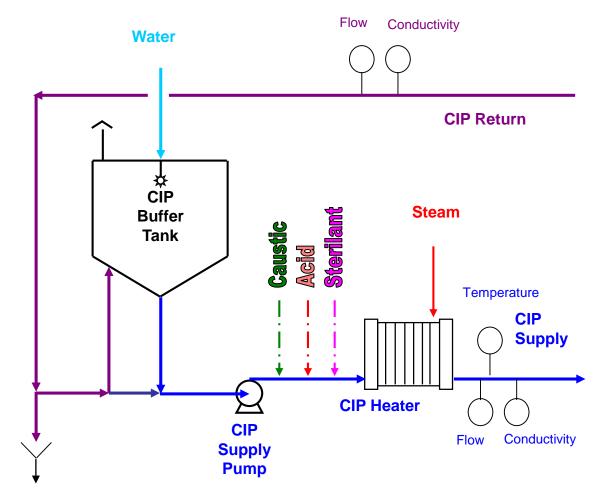


# **CIP** Systems

- Single Use
  - Water/Effluent/Energy costs
- Recovery
  - Detergent Recovery
  - Rinse/Interface Recovery
- Tank Allocation
- Number of Circuits

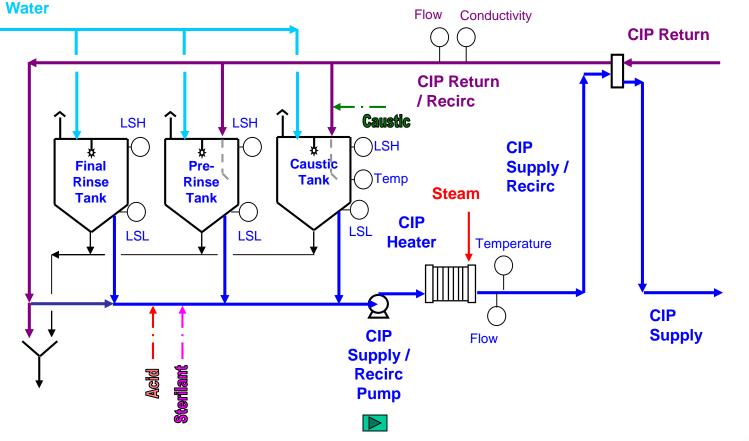


# Single Use CIP Systems





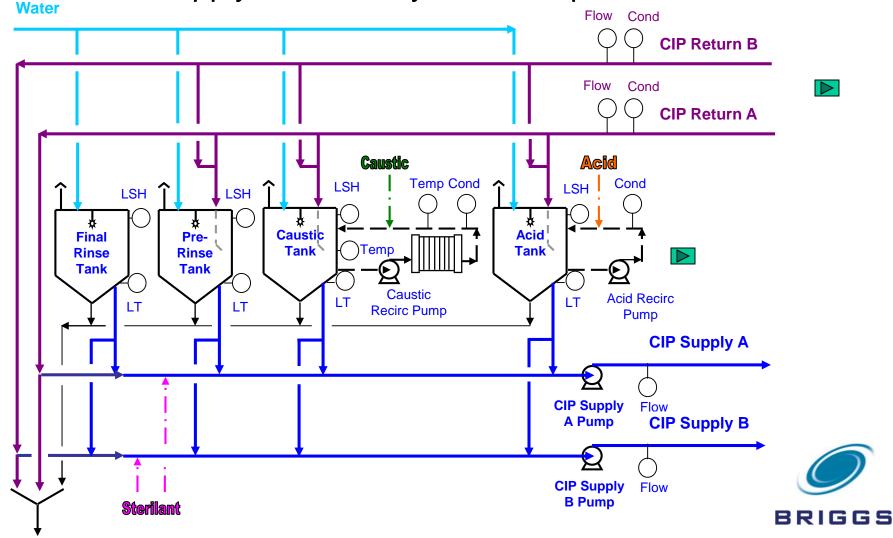
#### Recovery CIP Systems 1 x Supply – 3 Tank System





## **Recovery CIP Systems**

2 x Supply – 4 Tank System – Separate Recirc



## **Recovery CIP System**





# Single Use vs Recovery

- Single Use CIP
  - Low Capital Cost
  - Small Space Req.
  - Low Contamination Risk
  - Total Loss
    - High Water Use
    - High Energy Use
    - High Effluent Vols.
  - Longer Time/Delay
  - Use for Yeast

- Recovery CIP
  - High Capital Cost
  - Large Space Req.
  - Higher Contamination Risk
  - Low Loss
    - Low Water Use
    - Low Energy Use
    - Low Effluent Vols.
  - Shorter Time/Delay
  - Use for Brewhouse & Fermenting



# CIP Systems CIP Tank Sizing

- Pre-Rinse
  - CIP Flow x Time
- Detergent
  - Vol of CIP in Process Mains & Tank
     + Losses
- Final Rinse
  - Flow x Time Water Fill



## CIP Systems Practical Points

- CIP Supply Pump
- Recirculation
- Shared/Common with CIP Supply, or
- Dedicated to Tank
- CIP Supply Strainer
- CIP Return Strainer
- CIP Tank Connections



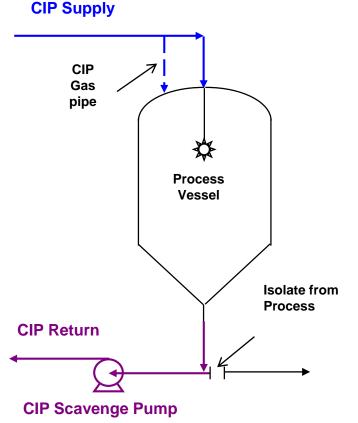
# Types of CIP

- VESSEL CIP
  - Sprayhead Selection
  - Scavenge Control
- MAINS CIP
  - Adequate Velocity
  - Total Route Coverage
- BATCH/COMBINED CIP
  - Complex Control
  - Time Consuming



#### Vessel CIP

- Flow of CIP fluid from CIP supply to vessel sprayhead
- Internal surfaces cleaned by spray impact / deluge
- Return from vessel by CIP scavenge (return) pump





# Vessel CIP - Sprayheads

- Static Sprayballs

   High Flow / Low Pressure
- Rotating Sprayheads

   Low Flow / Medium Pressure
- Cleaning Machines
  - Low Flow / High Pressure
  - High Impact



## Vessel CIP – Sprayballs

- Advantages
  - No moving parts
  - Low Capital Cost
  - Low pressure CIP supply
  - Verification by Flow
- Disadvantages
  - High Water & Energy Use
  - High Effluent volumes
  - Limited throw Small vessels
  - Spray Atomises if Pressure High
  - No impact long CIP time and/or high detergent strength
  - Higher absorption of CO<sub>2</sub> by caustic





# Vessel CIP – Rotary Sprayheads

- Advantages
  - Not too Expensive
  - Some Mechanical Soil Removal
  - Lower Flow
  - Reasonable Water/Energy Usage
  - Reasonable Effluent
- Disadvantages
  - Moving parts
  - Limited throw Small vessels
  - Possible blockage
    - Rotation verification
    - Supply strainer







# Vessel CIP – Cleaning Machines

- Advantages
  - High impact, aggressive cleaning
  - Good for heavy duty cleaning
  - Low water/energy use
  - Low effluent
  - Effective in large vessels
  - Lower absorption of CO2 by caustic
  - Lower Flow means smaller Pipework





# Vessel CIP – Cleaning Machines

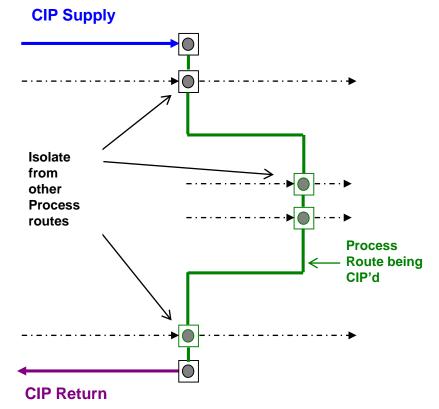
- Disadvantages
  - Expensive
  - Moving parts
  - High pressure CIP supply pump
  - Possible blockage
    - Rotation verification
    - Supply strainer





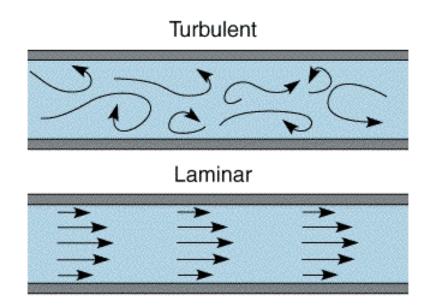
#### Mains CIP

- Flow of CIP fluid from CIP supply, through process pipework and back to CIP set
- The entire process
   route must see
   turbulent CIP Flow
- No/Minimal Tees/dead legs
- Isolate from other process lines





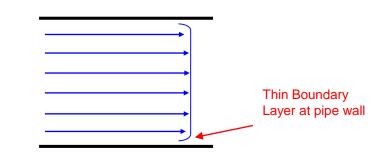
# Mains CIP Turbulent & Laminar Flow

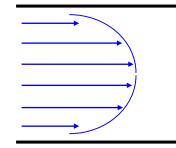




# Mains CIP Turbulent & Laminar Flow

- Turbulent Flow
  - Flat velocity profile
  - Thin Boundary layer
  - Effective CIP
- Laminar Flow
  - Streamline flow
  - Velocity profile, faster at centre
  - Ineffective CIP







### Mains CIP

- Turbulent Flow –
   Re > 3000
- Minimise Boundary layer –
   Laminar layer on internal pipe wall
- Minimum CIP velocity (in process pipe)  $\geq$  1.5 m/s.
- Excessive velocity

   High Pressure drop / Energy input



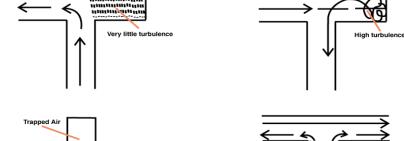
### Mains CIP – CIP Flow

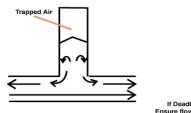
Process Pipe dia (mm)	Minimum CIP Flow (m <sup>3</sup> /h)	CIP Supply / Return dia (mm)
25	2.1	25
38	5.2	38
50	10	<b>50</b>
65	16	<b>65</b>
75	24	<mark>65</mark>
100	42	75
125	70	100
150	100	125
200	170	150
250	280	200
300	400	200
350	<b>520</b>	250
400	700	250
Min CIP Velocity	1.5	m/s minimum
Based on o/d tube to 100 mm and metric I/d above 100 mm.		



# Process Pipework Design for CIP

- Ensure Total Route coverage
  - Avoid Split routes
  - Avoid Dead ends
  - Avoid Tees
  - Most Critical on Yeast & nearer packaging





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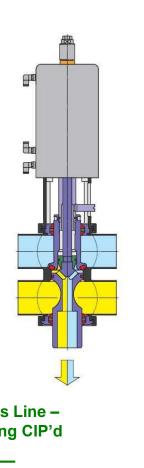
If Deadlegs are unavoidable∙ Ensure flow directed i<u>nto</u> dead end Dead end is as <u>short</u> as possible - L/D = 1.5



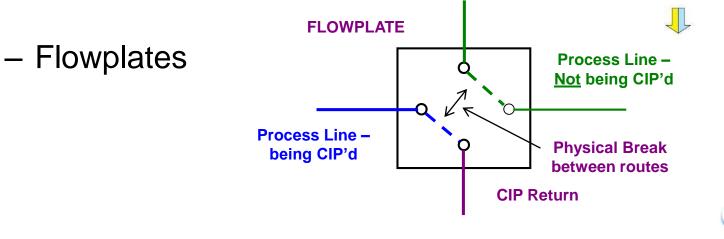
Potential Trape for soil debris

## Process Pipework Design for CIP

- Isolate CIP from Process
  - Mixproof Valves



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### Batch/Combined CIP

- Combines CIP of
  - Vessel/s and
  - Pipework in one clean
- Why ?
  - Pipework too large for 'mains' CIP
     e.g. Brewhouse 200 to 600 mm.
  - Pipework linked to Vessel
     e.g. Recirculation Loop or EWH.



### Batch/Combined CIP

- Supply of a batch volume of CIP to process vessel
- Internal recirculation of CIP within/through process vessel
- Transfer of CIP to next vessel
- Pumped return of CIP batch volume to CIP set.



# CIP Monitoring & Control On-Line

- Detergent Temperature
- Detergent Strength Conductivity
- Return Conductivity
  - Detergent Start Interface
  - Detergent End Interface
  - Rinse Conductivity
- Return Flow
- Recirc/Return Time
- Supply Pressure



# CIP Monitoring & Control Off-Line

- Visual Inspection
- Final Rinse return sampling
  - pH
  - Micro
  - ATP
- Vessel/Pipework swabs
  - pH
  - Micro
  - ATP



## Principles and Practice of Cleaning in Place

